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**GB-A- 2 185 517**  
**US-A- 3 954 678**  
**CHEMICAL ABSTRACTS, vol. 82, no. 22, 2nd**  
**June 1975, page 332, abstract no. 144992r,**  
**Columbus, Ohio, US.**

⑦③ Proprietor : **BROCADES PHARMA B.V.**  
**Eilsabethhof 19 P.O. Box 108**  
**NL-2350 AC Leiderdorp (NL)**

⑦② Inventor : **Komen, Joseph**  
**Ambachtstraat 8**  
**NL-2024 EB Haarlem (NL)**  
Inventor : **Groenendaal, Jan Willem**  
**Koommarkt 4**  
**NL-2611 EE Delft (NL)**

⑦④ Representative : **Lavy, Uriel et al**  
**Gist-Brocades NV Patents and Trademarks**  
**Dept. Wateringsweg 1 P.O. Box 1**  
**NL-2600 MA Delft (NL)**

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## Description

This invention relates to a process for microencapsulating bioactive substances in biocompatible polymers according to the phase-separation principle and to pharmaceutical compositions containing the microcapsules prepared by this process.

Microencapsulation of bioactive substances in biocompatible polymers is useful for the production of controlled-release preparations. The polymer used thereby determines the release characteristics of the bioactive substances. Biocompatible polymers which are also biodegradable are especially suitable for the production of injectable preparations.

Technologies of microencapsulation have been described by W. Fong in "Controlled Release Systems: Fabrication Technology" Vol. I Editor Dean Hsieh, CRD Press, Florida, 1988, chapter 5, page 81-108 "Microencapsulation by solvent evaporation and organic phase-separation processes". There it is disclosed, that the principle of phase-separation, as opposed to solvent-dispersion, is especially suitable for encapsulating hydrophilic bioactive substances, but that it is also applicable to water-insoluble ones. The products of encapsulation may be true, "heterogeneous", microcapsules wherein the polymer encapsulates the bioactive core. The products may also be "homogeneous microspheres", wherein the bioactive substance is dispersed in the polymer.

Microencapsulation by phase-separation of hydrophilic bioactive substances in biodegradable polymers has been disclosed in EP-A-0052510 and in GB-A-2165517. Microencapsulation of a hydrophilic bioactive substance in non-biodegradable polymers has been disclosed by S. Benita et al., J. Pharm. Pharmacol. 1985, 37, 391-395, "Microencapsulation of Paracetamol Using Polyacrylate Resins (Eudragit Retard)". These techniques generally comprise the following steps:

- a. Dispersing a bioactive substance in a solution (in an organic solvent which is not miscible with water) of a biocompatible polymer;
- b. Adding to the dispersion a so-called non-solvent (or coacervation agent), an organic liquid which is not miscible with the biocompatible polymer. This results in coacervation (or phase-separation), whereby the biocompatible polymer is deposited on the dispersed bioactive substance to form "embryonic" microcapsules;
- c. Extracting the residual organic solvent out of the "embryonic" microcapsules and hardening them by adding to the dispersion an excess, with respect to the combined volume of solvent and non-solvent, of a so-called hardening liquid;
- d. Collecting the hardened microcapsules from the dispersion, washing the microcapsules, and drying the microcapsules by any of the methods generally known in the art.

Hydrophilic bioactive substances which may be encapsulated by such processes are polypeptides such as luteinizing hormone, somatostatin and interferon. They are mostly dispersed in water before dispersing them in the organic solvent, but this is not always necessary (see e.g. GB-A-2165517). Lipophilic bioactive compounds such as steroids can also be encapsulated.

Biocompatible, biodegradable polymers which are known to be useful in encapsulating bioactive substances in such processes are polylactides, polyglycolides and copolymers of lactides and glycolides. Useful non-biodegradable biocompatible polymers are the pH-dependent polyacrylate resins such as EUDRAGIT®-S and the pH-independent polyacrylate resins such as EUDRAGIT®-RS and ethylcellulose.

Organic solvents which are miscible with the polymer and with the non-solvent while being immiscible with water are halogenated hydrocarbons, such as dichloromethane ( $\text{CH}_2\text{Cl}_2$ ).

Useful non-solvents are silicone oils.

The invention concerns in particular the step of hardening the microcapsules. The hardening liquid to be used in this step has to extract efficiently and fully any solvent and non-solvent from the microcapsules without dissolving the biodegradable polymer or the bioactive substance and without misforming the microcapsules or causing their aggregation. While the amount of any residues in the microcapsules has to be kept at a minimum, any residual amount of hardener has to be absolutely biocompatible.

Up to now only a very limited number of liquids has actually been used as hardening liquid.

EP-A-0052510 discloses as hardening liquids alkane organic solvents such as heptane. GB-A-2165517 points out that these compounds tend to leave a substantial amount of residue in the ready capsules, and that they are inflammable and/or toxic. Therefore GB-A-2165517 is directed to the use as hardening liquids of fluor- or fluorhalogen hydrocarbons, such as those known under the general name Freon®, which are stated to leave a smaller amount of residue and to be less toxic. However, the amount of residue is actually still substantial and these compounds are not in general use for systemic medical applications other than inhalation and they have not been cleared and declared free of toxicity. Also, while GB-A-2165517 recommends the application of these compounds in the preparation of microcapsules based on a variety of biocompatible, biodegradable

polymers, for example those of L-lactide, DL-lactide and the copolymers of DL-lactide and glycolide, only the latter, in a 2% solution, were actually used in the six examples of GB-A-2165517. Extensive attempts to prepare microcapsules according to GB 2165517 using both Freon 113® (1,1,2 trichlorotrifluoroethane) and Freon 11® (trichlorofluoromethane) as the hardening liquids and DL-lactide as the biocompatible polymer in both 2% and 10% w/w solution, have all ended in failure of the microcapsules to harden.

It has now been found that ethyl and isopropyl esters of straight-chain fatty acids having 12-18 carbon atoms are outstandingly effective as hardening liquids for use in preparing microcapsules according to the phase-separation principle. Examples of such compounds are ethyl stearate, isopropyl stearate, ethyl oleate and preferably isopropyl myristate and isopropyl palmitate. Isopropyl myristate is the most preferred hardening liquid according to the invention, being the most versatile in its uses.

Isopropyl myristate and isopropyl palmitate are both in use as dermatological excipients and are known to have a very low order of toxicity. E.g. attempts to establish an LD<sub>50</sub> of isopropyl myristate in mice failed when dosages equivalent to 100 ml/kg did not affect the animals. Therefore these compounds are considered fully biocompatible. Moreover, they are not inflammable, nor are they detrimental to the environment.

The invention is therefore characterized in that in the step of hardening the microcapsules the hardening liquid is an ethyl or isopropyl ester of a straight-chain fatty acid having 12-18 carbon atoms or a mixture thereof.

Preferably, the volume of the hardening liquid used according to the invention is between 5-25 times the total volume of solvent and non-solvent.

In order to prevent the formation of microcapsules of irregular shape, the temperature during the hardening process is preferably kept between 3 and 25°C. More preferably the temperature is kept between 3 and 10°C when isopropyl myristate or isopropyl palmitate are used for hardening poly-(DL-lactide-co-glycolide) or poly-L-lactide, and between 18 and 25°C when poly-DL-lactide is to be hardened.

Optionally the microcapsules can be washed after the step of adding the hardening liquid.

It will be appreciated that in principle all kinds of hydrophilic and lipophilic bioactive substances can be encapsulated in microcapsules according to the invention, especially when prolonged action is desired. Examples of hydrophilic bioactive substances are hormones and hormone-releasing factors and medicaments with anti-inflammatory, anti-peptic ulcer, anti-tumorous, anti-depressive, anti-hypertensive or antibiotic action. In particular peptides and proteins are suitable to be used as the hydrophilic bioactive compounds, such as adrenocorticotrophic hormones, angiotensins, blood clotting factors (factor VII, factor VIII), calcitonins, corticotrophin-releasing factors, cellular growth-regulating factors (EGF, TGF- $\alpha$  and - $\beta$ ), endorphins, enkephalins, gastrin inhibitory peptides, gastrins, gastrin releasing peptides, growth hormones, hemopoietic factors (IL-3, IL-6, CSF's and EPO), insulins, interferons, oxytocin, parathyroid hormones, somatostatin and vasopressins, and pharmacologically active analogues and fragments thereof.

Examples of lipophilic bioactive substances which can be microencapsulated according to the invention are the steroids. In particular the invention is useful for encapsulating bedomethasone 17,21-dipropionate, intended for controlled-release oral preparations against disorders of the intestine.

Further specific examples of bioactive substances which can be microencapsulated according to the invention are 4- and 5-amino-salicylic acid and Colloidal Bismuth Subcitrate.

The invention also includes the microcapsules prepared according to the described process as well as the preparations, such as pharmaceutical preparations, which contain these microcapsules in a suitable carrier. In particular the invention includes injectable pharmaceutical preparations, in which the microcapsules are dispersed in a suitable liquid carrier, and oral pharmaceutical preparations, in which the microcapsules are dispersed in a suitable carrier.

The invention is illustrated by the following Examples.

#### Example 1

##### Encapsulation of BSA in aqueous solution, in poly-L-lactide

100 mg of BSA (Sigma, art No. A 7030), were dissolved in 0.8 ml water. This solution, was added to a 300 ml Erlenmeyer containing 100 ml of a 2% solution of poly-L-lactide (Boehringer Ingelheim, lot No. EC 8707, mean mol weight 220,000, inh. visc. 1.82 dl/g, in CHCl<sub>3</sub> at 25°C) in dichloromethane. After 2 minutes of stirring (1000 RPM), 60 ml of silicone oil (Wacker AK 1000), were added while stirring, after which stirring was continued for another 15 minutes (300 rpm). The content of the Erlenmeyer was then poured into 1800 ml of isopropyl myristate (Henkel) at 5°C, which were also stirred (850 rpm) during a further 90 minutes, after which the microcapsules were sieved out of the liquid, using a sequence of 100, 50 and 25  $\mu$ m sieves. Finally, the microcapsules were washed and dried.

The collected microcapsules were freely flowable, and on microscopical inspection they were seen to be

generally spherical in form and to contain droplets of about 1-10  $\mu\text{m}$ , evenly dispersed over the spherules. The amounts of microcapsules collected over the three sieves were:

5	<u>Microcapsule size</u>	<u>amount collected</u>
	25 - 50 $\mu\text{m}$	223 mg
	50 - 100 $\mu\text{m}$	354 mg
	> 100 $\mu\text{m}$	<u>780 mg</u>
10		1357 mg

The content of BSA in the microcapsules was determined according to M.M. Bradford (Analyt. Biochem. 72 (1976) 248-254) and found to be 2.40% w/w, corresponding to a total content of BSA in the harvested microcapsules of 33 mg. This is a yield of 33% of encapsulated BSA.

#### Example 2

##### Encapsulation of dry BSA, in poly-(DL-lactide-co-glycolide)

100 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide 50:50 (Boehringer Ingelheim, lot No. EC 8713, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in  $\text{CHCl}_3$  at 25°C) were added to 800 mg of BSA (Sigma, art. No. A 7030, sieved fraction of 2-21  $\mu\text{m}$  particle size) in a dry reaction vessel, while stirring 1200 rpm for 5 minutes. Subsequently, while stirring at 400 rpm, 50 ml of silicone oil (Wacker AK 2000) were added during 1 minute, after which stirring was continued for another 5 minutes at 200 rpm. The content of the reaction vessel was then poured into 2000 ml of Isopropyl myristate (Henkel) at 5°C, which were also stirred (850 rpm) during a further 2 hours, after which the microcapsules were sieved out of the liquid using a 25  $\mu\text{m}$  sieve. The microcapsules were then washed, sieved again using a sequence of 140 and 25  $\mu\text{m}$  sieves and dried.

The collected microcapsules were freely flowable. On microscopic inspection they were seen to be indented spherules. Their size was between 25 and 140  $\mu\text{m}$  and their total yield 8500 mg, which is about 85 %. The content of BSA in the microcapsules was determined according to M.M. Bradford and found to be 4.73% w/w, corresponding to a total content of BSA in the harvested microcapsules of 402 mg. This is a yield of 50.2% of encapsulated BSA.

#### Example 3

##### Encapsulation of dry BSA in poly-DL-lactide

Microcapsules were prepared using similar steps as in Example 2, with the following modifications:

The polymer was poly-DL-lactide (CCA-Biochem, lot No. C059, mean mol weight 19.000) as a 10% solution in dichloromethane.

The non-solvent was Dow Corning silicone oil DC 200 fluid 200 cSt.

Isopropyl myristate was used in an amount of 2500 ml at 20°C.

The collected microcapsules were moderately sticky. They were spherical in form, and between 25 and 140  $\mu\text{m}$  in size. Their total yield was 7900 mg, which is about 80%. The content of BSA in the microcapsules was determined according to M.M. Bradford and found to be 3.5 w/w, corresponding to a total content of BSA in the harvested microcapsules of 276 mg. This is a yield of 43.8% of encapsulated BSA.

#### Example 4

##### Encapsulation of dry BSA in poly-(DL-lactide-co-glycolide). Hardening liquid: ethyl laurate

32 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide) 50:50 (Resomer® RG 505, lot No. EC8713, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in  $\text{CHCl}_3$  at 25°C) were added to 150 mg of BSA (Sigma bovine serum albumin prod. No. A-7030, sieved fraction of 2-21  $\mu\text{m}$  part. size) in a 100 ml dry glass-beaker. BSA was dispersed by stirring at 1000 rpm for 5 minutes at room temperature. Subsequently, while stirring at 400 rpm, 16 ml of polydimethylsiloxane (Dow Corning DC 360, medical

grade, viscosity 2000 cSt) were added during 2 minutes. The content of the beaker was then added to 500 ml ethyl laurate (zur Synthese, Merck art. 805334), at 20°C, which were also stirred (400 rpm) during a further 16 hours, after which stirring was stopped. After sedimentation of the microcapsules the ethyl laurate was decanted. Then an amount of 250 ml ethanol was added and stirred for 16 hours at 400 rpm. After stopping stirring and decanting again, a fresh amount of 250 ml ethanol was added and stirred at 400 rpm during ten minutes. After the last washing procedure with ethanol, microcapsules were collected above a 10 µm Teflon® membrane filter by filtrating the ethanol. The microcapsules were dried during 24 hours under continuous vacuum conditions.

The total yield of microcapsules was 3.02 grams. The yield of 25-160 µm microcapsules was 2.86 grams which is about 85.4%.

The content of BSA was determined according to M.M. Bradford and found to be 2.3% w/w, corresponding to a total content of BSA in the harvested microcapsules of 0.066 gram BSA. This is a yield of 44.0% of encapsulated BSA.

#### Example 5

Encapsulation of dry insulin in poly-(DL-lactide-co-glycolide). Hardening liquid: isopropyl myristate

200 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide) 50:50 (Resomer® RG 505 Boehringer Ingelheim, lot No. EC7813, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in CHCl<sub>3</sub> at 25°C) were added to 1 gram of insulin (Sigma bovine insulin prod. No. I-5500, lot No. 38F-0827, 15 µm crystalline particles) in a 300 ml dry glass-beaker. The insulin was dispersed by stirring at 1200 rpm for 5 minutes at room temperature. Subsequently, while stirring at 400 rpm, 100 ml of polydimethylsiloxane (Dow Corning DC 360, medical grade, viscosity 2000 cSt) were added during 2 minutes. The content of the beaker was then added to 4000 ml Isopropyl myristate (Henkel), at 20°C, which were also stirred (400 rpm) during a further 24 hours, after which stirring was stopped. After sedimentation of the microcapsules the Isopropyl myristate was decanted. Then a fresh amount of 1000 ml isopropyl myristate was added and stirred for another 24 hours at 400 rpm. After stopping stirring and decanting again, 400 ml ethanol were added and stirred at 400 rpm during ten minutes. After decanting the ethanol, the washing procedure was repeated. After the last washing procedure with ethanol, microcapsules were collected above a 10 µm membrane filter by filtrating the ethanol. The microcapsules were dried during 24 hours under continuous vacuum conditions.

The total yield of microcapsules was 20 grams. The yield of 25-140 µm microcapsules was 19.5 grams which is about 93%.

The content of insulin was determined according to M.M. Bradford and found to be 3.9% w/w, corresponding to a total content of insulin in the harvested microcapsules of 0.760 gram insulin; this is a yield of 76.1% of encapsulated insulin.

#### Example 6

Encapsulation of dry insulin in poly-(DL-lactide-co-glycolide). Hardening Liquid: ethyl myristate

100 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide) 50:50 (Resomer® RG 505 Boehringer Ingelheim, lot No. EC8713, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in CHCl<sub>3</sub> at 25°C) were added to 500 mg of insulin (Sigma bovine insulin prod. No. I-5500, lot No. 38F-0827, 15 µm crystalline particles) in a 300 ml dry glass-beaker. The insulin was dispersed by stirring at 1000 rpm for 5 minutes at room temperature. Subsequently, while stirring at 400 rpm, 50 ml of polydimethylsiloxane (Dow Corning DC 360, medical grade, viscosity 2000 cSt) were added during 2 minutes. The content of the beaker was then added to 1500 ml ethyl myristate (zur Synthese, Merck art. 818970), at 20°C, which were also stirred (400 rpm) during a further 2 hours, after which stirring was stopped. After sedimentation of the microcapsules the ethyl myristate was decanted. Then a fresh amount of 500 ml ethyl myristate was added and stirred for another 24 hours at 400 rpm. After stopping stirring and decanting again, 400 ml ethanol were added and stirred at 400 rpm during ten minutes. After decanting the ethanol, the washing procedure was repeated twice. After the last washing procedure with ethanol, microcapsules were collected above a 10 µm Teflon® membrane filter by filtrating the ethanol. The microcapsules were dried during 24 hours under continuous vacuum conditions.

The total yield of microcapsules was 9.01 grams. The yield of 25-140 µm microcapsules was 8.41 grams which is about 80.0%.

The content of insulin was determined according to M.M. Bradford and found to be 3.5% w/w, corresponding to a total content of insulin in the harvested microcapsules of 0.294 gram insulin. This is a yield of 58.9% of

encapsulated insulin.

#### Example 7

##### 5 Encapsulation of dry Insulin in poly-(DL-lactide-co-glycolide). Hardening liquid: ethyl oleate

100 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide) 50:50 (Resomer® RG 505 Boehringer Ingelheim, lot No. EC8713, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in CHCl<sub>3</sub> at 25°C) were added to 500 mg of Insulin (Sigma bovine insulin prod. No. I-5500, lot No. 38F-0827, 15 µm crystalline particles) in a 300 ml dry glass-beaker. The insulin was dispersed by stirring at 1000 rpm for 5 minutes at room temperature. Subsequently, while stirring at 400 rpm, 50 ml of polydimethylsiloxane (Dow Corning DC 360, medical grade, viscosity 2000 cSt) were added during 2 minutes. The content of the beaker was then added to 1500 ml ethyl oleate at 20°C, which were also stirred (400 rpm) during a further 2 hours, after which stirring was stopped. After sedimentation of the microcapsules the ethyl oleate was decanted. Then an amount of 500 ml isopropyl myristate was added and stirred for another 24 hours at 400 rpm. After stopping stirring and decanting again, 400 ml ethanol were added and stirred at 400 rpm during ten minutes. After decanting the ethanol the washing procedure was repeated twice. After the last washing procedure with ethanol, microcapsules were collected above 10 µm Teflon® membrane filter by filtrating the ethanol. The microcapsules were dried during 24 hours under continuous vacuum conditions.

20 The total yield of microcapsules was 9.01 grams. The yield of 25-140 µm microcapsules was 8.2 grams which is about 78.0%.

The content of insulin was determined according to M.M. Bradford and found to be 3.5% w/w, corresponding to a total content of insulin in the harvested microcapsules of 0.287 gram Insulin. This is a yield of 57.4% of encapsulated Insulin.

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#### Example 8

##### Encapsulation of dry insulin in poly-(DL-lactide-co-glycolide). Hardening liquid: isopropyl palmitate

30 100 ml of a 10% solution in dichloromethane of poly-(DL-lactide-co-glycolide) 50:50 (Resomer® RG 505 Boehringer Ingelheim, lot No. EC8713, mean mol weight 91,000, inherent viscosity 0.7 dl/g, in CHCl<sub>3</sub> at 25°C) were added to 500 mg of insulin (Sigma bovine insulin prod. No. I-5500, lot No. 38F-0827, 15 µm crystalline particles) in a 300 ml dry glass-beaker. The insulin was dispersed by stirring at 1000 rpm for 5 minutes at room temperature. Subsequently, while stirring at 400 rpm, 50 ml of polydimethylsiloxane (Dow Corning DC 360, medical grade, viscosity 2000 cSt) were added during 2 minutes. The content of the beaker was then added to 1500 ml isopropyl palmitate (Henkel cospha products, lot 727067), at 20°C, which were also stirred (400 rpm) during a further 16 hours, after which stirring was stopped. After sedimentation of the microcapsules the isopropyl palmitate was decanted. Then an amount of 500 ml isopropyl myristate was added and stirred for 10 minutes at 400 rpm. After stopping stirring and decanting again, 400 ml ethanol were added and stirred at 400 rpm during ten minutes. After decanting the ethanol the washing procedure was repeated twice. After the last washing procedure with ethanol, microcapsules were collected above 10 µm Teflon® membrane filter by filtrating the ethanol. The microcapsules were dried during 24 hours under continuous vacuum conditions.

The total yield of microcapsules was 9.81 grams. The yield of 25-140 µm microcapsules was 3.10 grams which is about 30%.

45 The content of insulin was determined according to M.M. Bradford and found to be 3.4% w/w, corresponding to a total content of insulin in the harvested microcapsules of 0.105 gram Insulin. This is a yield of 21.1% of encapsulated Insulin.

#### Example 9

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##### Encapsulation of beclomethasone 17,21-dipropionate in EUDRAGIT-RL. Hardening Liquid: isopropyl myristate

30 ml of a 10% solution in dichloromethane of EUDRAGIT®-RL-100 were added to 0.333 g of beclomethasone 17,21-dipropionate in a 100 ml glass-beaker. The beclomethasone dipropionate was dissolved by stirring at 250 rpm at room temperature. Subsequently, while stirring at 250 rpm, 30 ml of polydimethylsiloxane (Wacker AK-1000, viscosity 1000 cSt) were added during 1 minute. The content of the beaker was then added to 500 ml isopropyl myristate (Henkel), at 20°C, which were also stirred at 250 rpm during a further 24 hours,

after which stirring was stopped. After sedimentation of the microcapsules the isopropyl myristate was decanted. The microcapsules were washed twice with 200 ml of n-hexane and collected above a 10 µm membrane filter. The microcapsules were then dried during 24 hours at room temperature.

The total yield of microcapsules was 3 grams, which is about 90%. The content of the beclomethasone 17,21-dipropionate as determined by HPLC was 7.9% w/w, corresponding to a total content of beclomethasone 17,21-dipropionate in the harvested microcapsules of 0.24 g, which is a yield of 72% w/w.

#### Example 10

##### Residual content of different hardening liquids in microcapsules

The residual content of Isopropyl myristate in the microcapsules, prepared according to Example 2, was determined by Thin Layer chromatography and found to be 5% w/w.

The residual content of heptane in microcapsules, prepared according to Example 2 (Isopropyl myristate replaced by heptane) was determined by Gas Liquid chromatography and found to be approximately 8% w/w.

The residual contents of Freon 113 and Freon 11 in microcapsules, prepared according to Example 2 of GB-A-2165517, were determined by gas-liquid chromatography and found to be 24% w/w and 19% w/w, respectively.

#### Example 11

##### Release of BSA from microcapsules

Ten samples of 50 mg of microcapsules, prepared according to Example 2, were placed each in 100 ml of phosphate buffer, pH 7.4, to which was added 100 mg of sodium azide. The vessels were kept during their follow-up periods at 37°C and shaken at a rate of 37.5 cycles per minute. At different time intervals up to 28 days the complete microcapsules-content from one vessel was analysed for its residual BSA content, using the method of M.M. Bradford. The reciprocal results (dissolved BSA) are presented in figure 1 and show an approximately linear release of BSA up to 70% at 28 days.

#### Example 12

##### Release of insulin from microcapsules

Nine samples of 60 mg of microcapsules, prepared according to Example 5, were placed each in 100 ml of phosphate buffer, pH 7.4, to which were added 372 mg of sodium EDTA and 100 mg of sodium azide. The vessels were kept during their follow-up periods at 37°C and shaken at a rate of 37.5 cycles per minute. At different time-intervals up to 60 days the complete microcapsules-content from one vessel was analysed for its residual insulin content, using the method of M.M. Bradford.

The reciprocal results (dissolved insulin) are presented in figure 2 and show an approximately linear release of insulin up to almost 100% at 50 days.

#### Example 13

##### Release of beclomethasone 17,21-dipropionate from microcapsules

40 mg of microcapsules, prepared according to Example 9, were placed in 500 ml of phosphate buffer, pH 7, to which was added 1% of CETOMACROGOL® 1000.

The USP-paddle dissolution system was used with a stirring speed of 100 rpm. The temperature was 37°C. At time intervals up to 48 hours a 1.5 ml sample was taken and filtered, and its beclomethasone 17,21-dipropionate content determined by HPLC against a standard of 6 µg/ml of beclomethasone 17,21-dipropionate in phosphate buffer of pH 7, containing 2% of CETOMACROGOL® 1000.

The mean results of 3 determinations, as shown in figure 3, clearly demonstrate a sustained release.

**Example 14****Encapsulation of 5-amino-salicylic acid in EUDRAGIT®RS. Hardening liquid: isopropyl myristate**

5 100 ml of a 6% solution in dichloromethane of EUDRAGIT®-RS-100 were added to 20 g of 5-amino-salicylic acid in a 300 ml vessel. The 5-amino-salicylic acid was suspended by stirring at 250 rpm at room temperature. Subsequently, while stirring at 250 rpm, 100 ml of polydimethylsiloxane (Dow Corning DC 360, viscosity 1000 cSt) were added during 1 minute. After sedimentation of the microcapsules in-situ the liquid was decanted. The residual content of the vessel was then added to 800 ml isopropyl myristate (Henkel), at 20°C,  
 10 which were stirred at 500 rpm during a further 24 hours, after which stirring was stopped. After sedimentation of the microcapsules the isopropyl myristate was decanted. The hardened microcapsules were washed twice with 200 ml of n-heptane and collected above a 10 µm membrane filter. The microcapsules were then dried during 24 hours at room temperature.

The total yield of microcapsules was 20 grams, which is about 77%.

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**Example 15****Encapsulation of Colloidal Bismuth Subcitrate in ethylcellulose. Hardening liquid: isopropyl myristate**

20 The same procedure as described in Example 14 was carried out by using 20 g of Colloidal Bismuth Subcitrate as the biological active substance, ethylcellulose N22 as the non-biodegradable polymer, and polydimethylsiloxane (Dow Corning DC360, viscosity 2000 cSt) as the coacervation agent.

The total yield of microcapsules was 21.6 grams, which is about 83%.

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**Example 16****Release of 5-amino-salicylic acid from microcapsules**

340 mg of microcapsules, prepared according to Example 14, were placed in 1000 ml of phosphate buffer, pH 7.5, to which was added 0.1% PLURONIC® F-68.  
 30 The USP-paddle dissolution system was used with a stirring speed of 100 rpm. The temperature was 37°C. At time intervals up to 12 hours the absorbance at 326 nm was measured using a spectrophotometer equipped with a continuous-flow sampling system.

The 5-amino-salicylic acid content was calculated using the absorbance value of a standard of 260 µg/ml of 5-amino-salicylic acid in phosphate buffer of pH 7.5, containing 0.1% PLURONIC® F-68.  
 35 The results, as shown in figure 4, clearly demonstrate a sustained release.

**Claims**

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1. A process for microencapsulating bioactive substances according to the phase-separation principle, comprising the following steps:
  - a. dispersing the bioactive substance in an organic solution of a biocompatible polymer;
  - b. adding to the dispersion a coacervation agent (non-solvent)
  - 45 c. adding an excess, with respect to the combined volume of solvent and non-solvent, of a hardening liquid;
  - d. collecting, washing and drying the microcapsules, characterized in that the hardening liquid is an ethyl or isopropyl ester of a straight-chain fatty acid having 12-18 carbon atoms, or a mixture thereof.
- 50 2. A process according to claim 1, characterized in that the hardening liquid is isopropyl myristate or isopropyl palmitate.
3. A process according to claim 1 or 2, characterized in that the volume of hardening liquid used is 5-25 times the combined volume of solvent and non-solvent.
- 55 4. A process according to any of claims 1-3, characterized in that as the bioactive substance a hydrophilic substance is used.



5. A process according to claim 4, characterized in that as the hydrophilic substance a peptide or protein is used.
6. A process according to claim 5, characterized in that the peptide or protein is chosen from the group of  
adrenocorticotrophic hormones, angiotensins, blood clotting factors, calcitonins, corticotrophin-releasing  
factors, cellular growth-regulating factors, endorphins, enkephalins, gastrin inhibitory peptides, gastrins,  
gastrin releasing peptides, hemopoietic factors, growth hormones, insulins, interferons, oxytocin, para-  
thyroid hormones, somatostatin and vasopressins, and pharmacologically active analogues and frag-  
ments thereof.
7. A process according to claim 4, characterized in that as the hydrophylic substance Colloidal Bismuth Sub-  
citrate is used.
8. A process according to claim 4, characterized in that as the hydrophylic substance 4- or 5-amino-salicylic  
acid is used.
9. A process according to any of claims 1-3, characterized in that as the bioactive substance a lipophilic sub-  
stance is used.
10. A process according to claim 9, characterized in that as the lipophilic bioactive substance a steroid is used.
11. A process according to claim 10, characterized in that as the steroid beclomethasone 17,21-dipropionate  
is used.
12. A process according to any one of claims 1-11, characterized in that as the biocompatible polymer a bio-  
degradable polymer is used.
13. A process according to claim 12, characterized in that as the biodegradable polymer a poly-L-lactide, a  
poly-D,L-lactide or a copolymer of D,L-lactide and glycolide is used.
14. A process according to any one of claims 1-11, characterized in that as the biocompatible polymer a non-  
biodegradable polymer is used.
15. A process according to claim 14, characterized in that as the non-biodegradable polymer ethylcellulose,  
EUDRAGIT-RL, -RS, -NE, -L, or -S, hydroxypropyl methylcellulose phthalates, cellulose acetate phtha-  
lates, cellulose acetate trimellitate, polyvinyl acetate phthalate or shellac is used.
16. Microcapsules, prepared according to any one of claims 1-15.
17. A pharmaceutical preparation, in which microcapsules according to claim 16 are dispersed in a suitable  
carrier.
18. Injectable pharmaceutical preparations, in which microcapsules according to claim 16 are dispersed in a  
suitable liquid carrier.
19. Oral pharmaceutical preparations, in which microcapsules according to claim 16 are dispersed in a suit-  
able carrier.

#### Patentansprüche

1. Verfahren zur Mikroverkapselung bioaktiver Substanzen gemäss dem Phasen-Trennungs-Prinzip, das  
die folgenden Stufen umfasst:
  - a. Dispergieren der bioaktiven Substanz in einer organischen Lösung eines biokompatiblen Polymeren;
  - b. Zugabe zu der Dispersion eines Koazervationsmittels (Nichtlösers);
  - c. Zugabe eines Ueberschusses, bezogen auf das Gesamtvolumen von Lösungsmittel und Nichtlöser,  
einer Härtnungsflüssigkeit;
  - d. Sammeln, Waschen und Trocknen der Mikro kapseln, dadurch gekennzeichnet, dass die Härtnungs-  
flüssigkeit ein Ethyl- oder Isopropylester einer unverzweigten Fettsäure mit 12 bis 18 Kohlenstoffato-  
men oder ein Gemisch davon ist.

2. Verfahren nach Anspruch 1, dadurch gekennzeichnet, dass die Härtingsflüssigkeit Isopropylmyristat oder Isopropylpalmitat ist.
3. Verfahren nach Anspruch 1 oder 2, dadurch gekennzeichnet, dass das verwendete Volumen der Härtingsflüssigkeit das 5- bis 25-fache des Gesamtvolumens von Lösungsmittel und Nichtlöser ist.
4. Verfahren nach einem der Ansprüche 1 bis 3, dadurch gekennzeichnet, dass als bloaktive Substanz eine hydrophile Substanz verwendet wird.
5. Verfahren nach Anspruch 4, dadurch gekennzeichnet, dass als hydrophile Substanz ein Peptid oder Protein verwendet wird.
6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, dass das Peptid oder Protein gewählt ist aus der Gruppe von adrenokortikotropen Hormonen, Angiotensinen, Blutgerinnungsfaktoren, Kalzitonen, Kortikotropin-Freisetzungsfaktoren, Zellwachstums-Regulierungsfaktoren, Endorphinen, Enkephalinen, Gastrin-hemmenden Peptiden, Gastrinen, Gastrinfreisetzenden Peptiden, blutbildenden Faktoren, Wachstumshormonen, Insulinen, Interferonen, Oxytocin, Nebenschilddrüsenhormonen, Somatostatin und Vasopressinen und pharmakologisch aktiven Analogen und Fragmenten davon.
7. Verfahren nach Anspruch 4, dadurch gekennzeichnet, dass als hydrophile Substanz "Colloidal Bismuth Subcitrate" verwendet wird.
8. Verfahren nach Anspruch 4, dadurch gekennzeichnet, dass als hydrophile Substanz 4- oder 5-Aminosalicylsäure verwendet wird.
9. Verfahren nach einem der Ansprüche 1 bis 3, dadurch gekennzeichnet, dass als bloaktive Substanz eine lipophile Substanz verwendet wird.
10. Verfahren nach Anspruch 9, dadurch gekennzeichnet, dass als lipophile bloaktive Substanz ein Steroid verwendet wird.
11. Verfahren nach Anspruch 10, dadurch gekennzeichnet, dass als Steroid Beclometason-17,21-dipropionat verwendet wird.
12. Verfahren nach einem der Ansprüche 1 bis 11, dadurch gekennzeichnet, dass als biokompatibles Polymer ein biologisch abbaubares Polymer verwendet wird.
13. Verfahren nach Anspruch 12, dadurch gekennzeichnet, dass als biologisch abbaubares Polymer ein Poly-L-lactid, ein Poly-D,L-lactid oder ein Copolymer von D,L-Lactid und Glycolid verwendet wird.
14. Verfahren nach einem der Ansprüche 1 bis 11, dadurch gekennzeichnet, dass als biokompatibles Polymer ein nicht biologisch abbaubares Polymer verwendet wird.
15. Verfahren nach Anspruch 14, dadurch gekennzeichnet, dass als nicht biologisch abbaubares Polymer Ethylcellulose, EUDRAGIT-RL, -RS, -NE, -L oder -S, Hydroxypropylmethylcellulosephthalate, Celluloseacetatphthalate, Celluloseacetattrimellitat, Polyvinylacetatphthalat oder Schellack verwendet wird.
16. Mikrokapseln, hergestellt nach einem der Ansprüche 1 bis 15.
17. Pharmazeutisches Präparat, in dem Mikrokapseln nach Anspruch 16 in einem geeigneten Träger dispergiert sind.
18. Injizierbare pharmazeutische Präparate, in denen Mikrokapseln nach Anspruch 16 in einem geeigneten flüssigen Träger dispergiert sind.
19. Orale pharmazeutische Präparate, in denen Mikrokapseln nach Anspruch 16 in einem geeigneten Träger dispergiert sind.

## Revendications

1. Procédé de microencapsulation de substances bioactives suivant le principe de la séparation des phases, comprenant les stades suivants :
  - a. dispersion de la substance bioactive dans une solution organique d'un polymère biocompatible;
  - b. addition d'un agent de coacervation (non-solvant) à la dispersion;
  - c. addition d'un excès, par rapport au volume cumulé de solvant et de non-solvant, d'un liquide durcisseur;
  - d. collecte, de lavage et de séchage des microcapsules;
 caractérisé en ce que le liquide durcisseur est un ester éthylique ou isopropylique d'un acide gras à longue chaîne comptant 12 à 18 atomes de carbone, ou un mélange de ceux-ci.
2. Procédé suivant la revendication 1, caractérisé en ce que le liquide durcisseur est le myristate d'isopropyle ou le palmitate d'isopropyle.
3. Procédé suivant la revendication 1 ou 2, caractérisé en ce que le volume du liquide durcisseur utilisé est de 5 à 25 fois le volume cumulé du solvant et du non-solvant.
4. Procédé suivant l'une quelconque des revendications 1 à 3, caractérisé en ce qu'une substance hydrophile est utilisée comme substance bioactive.
5. Procédé suivant la revendication 4, caractérisé en ce qu'un peptide ou une protéine est utilisé comme substance hydrophile.
6. Procédé suivant la revendication 5, caractérisé en ce que le peptide ou la protéine est choisi dans la classe formée par les hormones adrénocorticotrophes, les angiotensines, les facteurs de coagulation du sang, les calcitonines, les facteurs de libération de la corticotrophine, les facteurs de régulation de la croissance cellulaire, les endorphines, les enképhalines, les peptides inhibiteurs des gastrines, les gastrines, les peptides libérateurs des gastrines, les facteurs hématopoïétiques, les hormones de croissance, les insulines, les Interférons, l'oxytocine, les hormones parathyroïdiennes, la somatostatine et les vasopressines, outre leurs analogues et fragments pharmacologiquement actifs.
7. Procédé suivant la revendication 4, caractérisé en ce que le sous-citrate de bismuth colloïdal est utilisé comme substance hydrophile.
8. Procédé suivant la revendication 4, caractérisé en ce que l'acide 4- ou 5-aminosalicylique est utilisé comme substance hydrophile.
9. Procédé suivant l'une quelconque des revendications 1 à 3, caractérisé en ce qu'une substance lipophile est utilisée comme substance bioactive.
10. Procédé suivant la revendication 9, caractérisé en ce qu'un stéroïde est utilisé comme substance bioactive lipophile.
11. Procédé suivant la revendication 10, caractérisé en ce que le 17,21-diproponate de bédométhasone est utilisé comme stéroïde.
12. Procédé suivant l'une quelconque des revendications 1 à 11, caractérisé en ce qu'un polymère biodégradable est utilisé comme polymère biocompatible.
13. Procédé suivant la revendication 12, caractérisé en ce qu'un poly-L-lactide, un poly-DL-lactide ou un copolymère de DL-lactide et de glycolide est utilisé comme polymère biodégradable.
14. Procédé suivant l'une quelconque des revendications 1 à 11, caractérisé en ce qu'un polymère non biodégradable est utilisé comme polymère biocompatible.
15. Procédé suivant la revendication 14, caractérisé en ce que l'éthylcellulose, l'EUDRAGIT-RL®, -RS, -NE, -L ou -S, les phtalates d'hydroxypropylméthylcellulose, les cétophtalates de cellulose, l'acétotrimellitate de cellulose, le poly(acétophtalate de vinyle) ou la gomme laque sont utilisés comme polymères non biodégradables.

- 16.** Microcapsules, préparées par un procédé suivant l'une quelconque des revendications 1 à 15.
- 17.** Préparation pharmaceutique, dans laquelle des microcapsules suivant la revendication 16 sont dispersées dans un excipient approprié.
- 5 18.** Préparation pharmaceutique injectable, dans laquelle des microcapsules suivant la revendication 16 sont dispersées dans un récipient liquide approprié.
- 10 19.** Préparation pharmaceutique à usage oral, dans laquelle des microcapsules suivant la revendication 16 sont dispersées dans un excipient approprié.

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FIG. 1

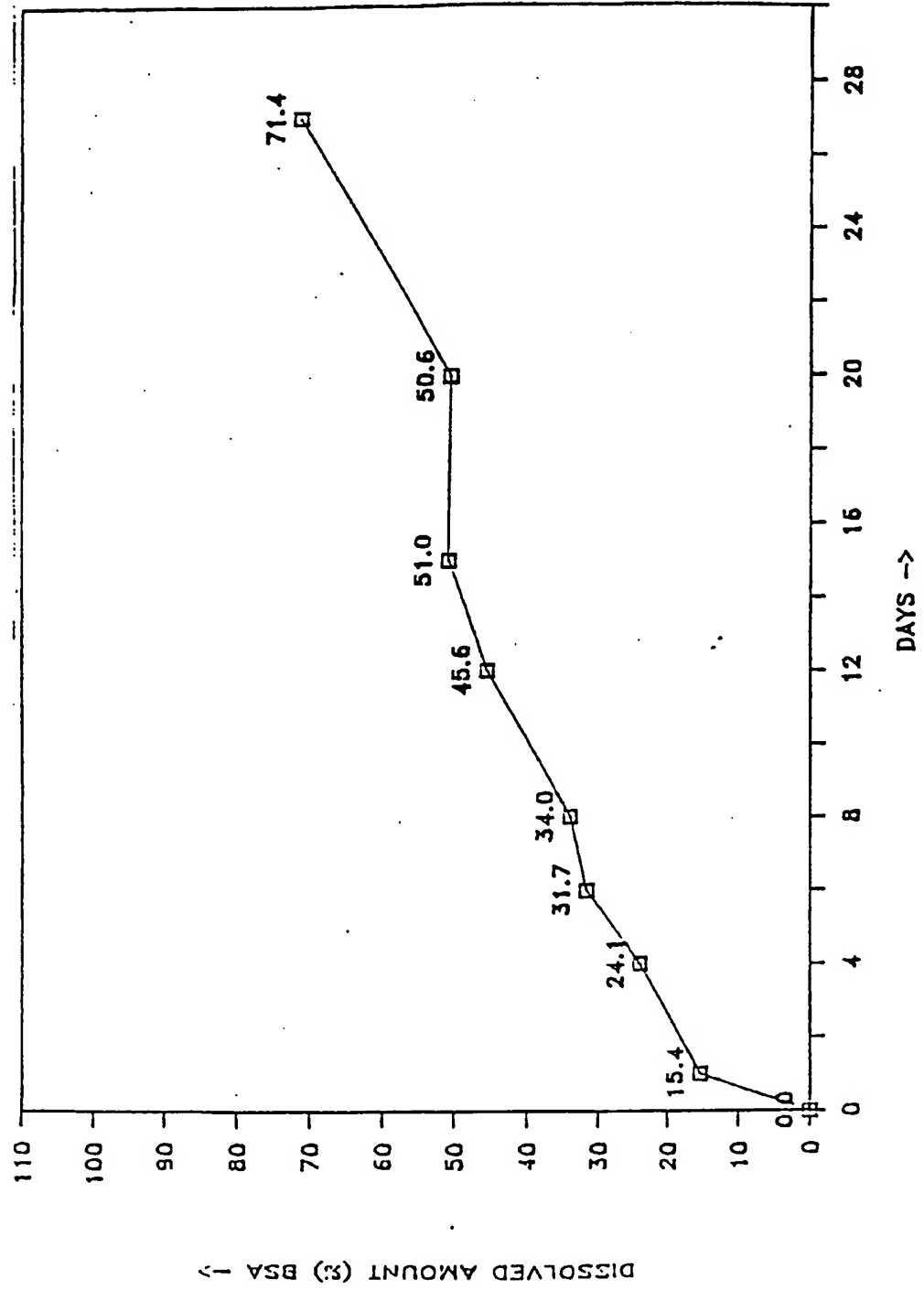


FIG. 2

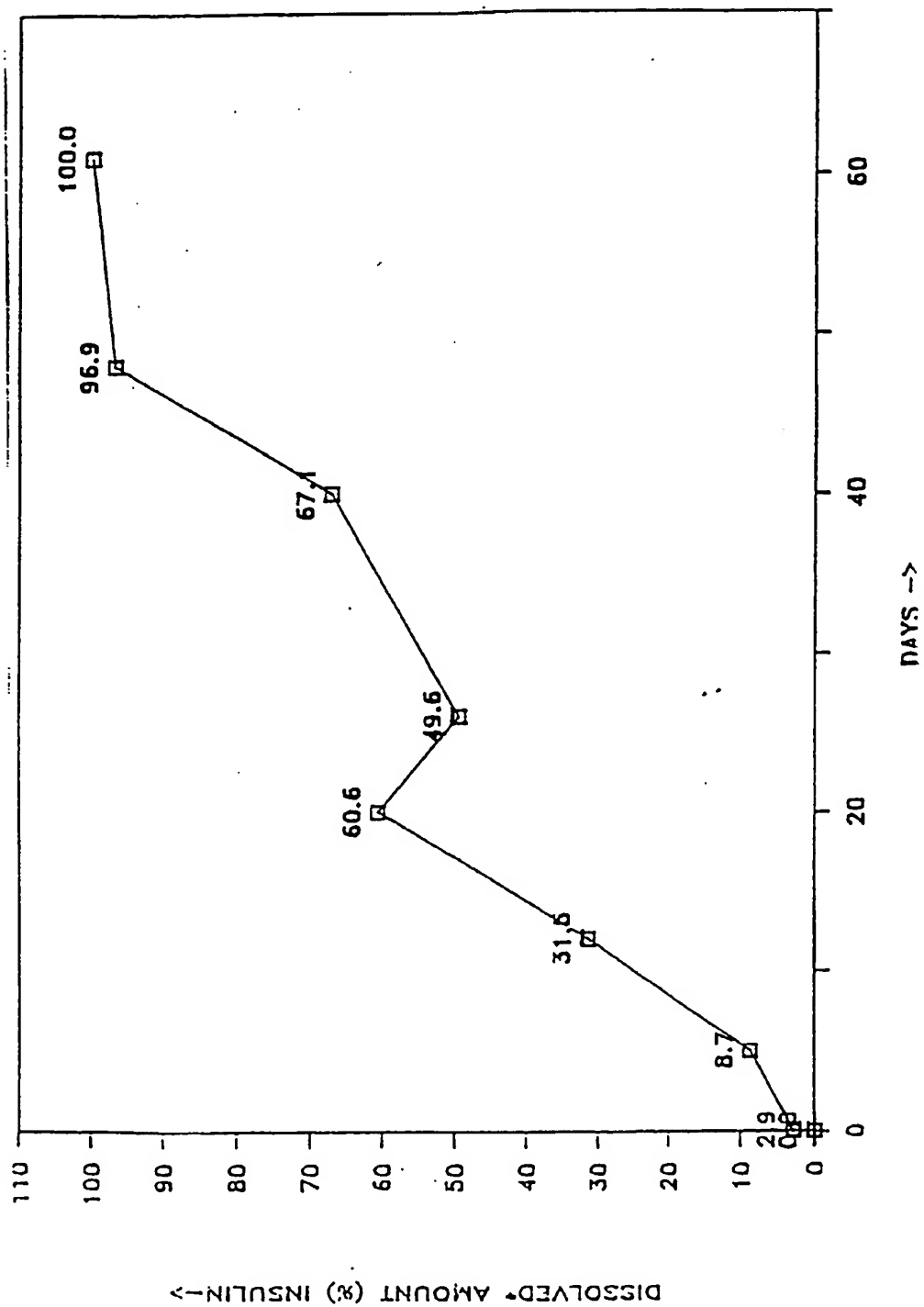


FIG. 3

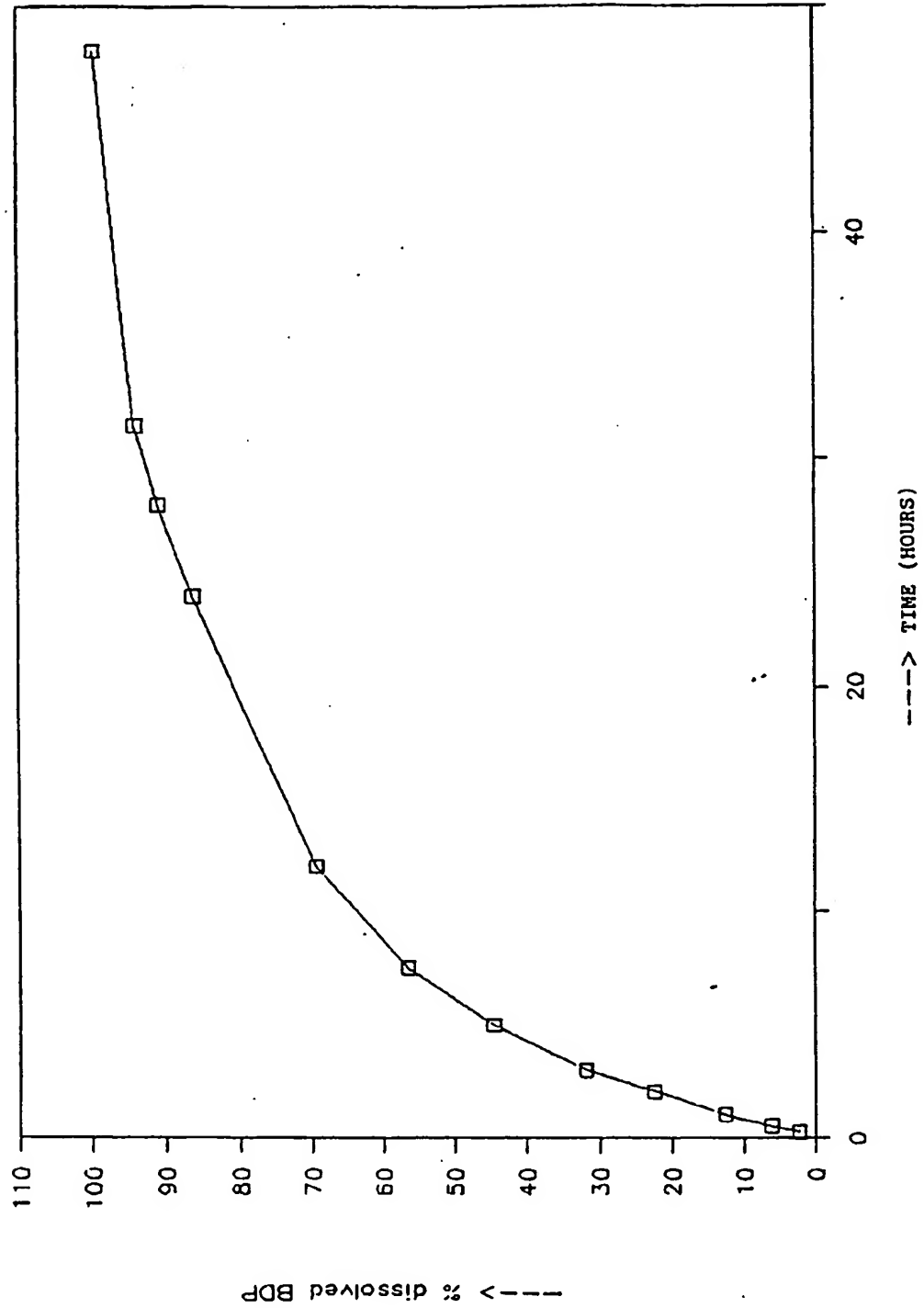


FIG. 4

